

5 **A METHOD AND CATALYST STRUCTURE FOR STEAM REFORMING
OF A HYDROCARBON**

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FIELD OF THE INVENTION

10 The present invention is a method and catalyst structure for steam reforming of a hydrocarbon.

BACKGROUND OF THE INVENTION

15 Steam reforming of hydrocarbons is commonly used for feedstock production for carbon-monoxide hydrogenation (Fischer-Tropsch synthesis), methanol synthesis and hydrogen production. Steam reforming is done commercially by flowing a mixture of steam and the hydrocarbon past a supported catalyst having an alumina support and a catalyst metal thereon, and
20 reacting the mixture at a temperature from about 600 °C to about 1000 °C, forming at least one product. Research has been done with the catalyst metal on a spinel support. Residence times are typically on the order of seconds and steam to carbon ratio greater than about 2.5. For steam to carbon ratio less than
25 formation and the supported catalyst must be refreshed or replaced.

30 The rate of supported catalyst activity degradation has been reduced by use of excess steam (steam to carbon ratio greater than 2.5). Excess steam, however, requires excess thermal energy and results in large system pressure drop. Using less steam results in faster degradation of catalyst activity because of coking from the hydrocarbon(s).

Hence, there is a need for a method of steam reforming of a hydrocarbon that provides greater product yield and permits using less steam and maintaining catalytic activity of the catalyst.

SUMMARY OF THE INVENTION

The present invention includes an improvement to the existing method of steam reforming of hydrocarbon, wherein the improvement comprises:

the flowing is at a rate providing a residence time less than about 0.1 sec resulting in obtaining product formation yield or amount that is the same or greater compared to product formation at a longer residence time.

Another improvement of the present invention is operation at a steam to carbon ratio that is substantially stoichiometric and maintaining activity of the supported catalyst.

The present invention also includes a catalyst structure for steam reforming of a hydrocarbon. The catalyst structure has

(a) a first porous structure with a first pore surface area and a first pore size of at least about 0.1 μm ;

(b) a porous interfacial layer that is a spinel with a second pore surface area and a second pore size less than the first pore size, the porous interfacial layer having a thickness less than 4 mm placed upon the first pore surface area;

(c) a steam reforming catalyst selected from the group consisting of rhodium, iridium, nickel, palladium, platinum, carbide of group VIb and combinations thereof placed upon the second pore surface area.

It is an object of the present invention to provide a method of steam reforming of hydrogen with a residence time of less than about 0.1 sec.

It is an object of the present invention to provide a catalyst structure with a porous interfacial layer of spinel.

The subject matter of the present invention is particularly pointed out and distinctly claimed in the concluding portion of this specification. However, both

the organization and method of operation, together with further advantages and objects thereof, may best be understood by reference to the following description taken in connection with accompanying drawings wherein like reference characters refer to like elements.

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BRIEF DESCRIPTION OF THE DRAWINGS

FIG. 1 is a graph of conversion and selectivity versus temperature.

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FIG. 2 is a graph of conversion and selectivity versus time.

DESCRIPTION OF THE PREFERRED EMBODIMENT(S)

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The present invention includes a method for steam reforming of a hydrocarbon having the steps of flowing a mixture of steam and the hydrocarbon past a supported catalyst having a support and a catalyst metal thereon. The mixture is reacted at a temperature from about 600 °C to about 1000 °C forming at least one product. The improvement of the present invention is using a spinel support and flowing the mixture at a rate providing a residence time less than about 0.1 sec and obtaining product formation that is the same or greater than that obtained at longer residence times.

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Also, under the previously described conditions, catalytic activity is degraded when the steam to carbon ratio is substantially stoichiometric. Another improvement of the present invention realized by flowing the mixture at a rate providing a residence time less than about 0.1 sec is maintaining activity of the spinel supported catalyst beyond 6 hours without degradation by coking even for substantially stoichiometric steam to carbon ratio. Substantially stoichiometric is a steam to carbon content ratio greater than about 0.9 and less than about 2.5, preferably from about 0.98 to about 2.

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The supported catalyst may be in the form of a powder of non-porous particles, porous solid and combinations thereof.

Hydrocarbon includes oxygenates, alkanes, alkenes, alkynes, branched isomers, aromatics, saturated and unsaturated hydrocarbons and combinations thereof including fuels such as gasoline, kerosine, diesel, JP-8.

5 Example 1

 An experiment was conducted to demonstrate the present invention. The supported catalyst was spinel of a gamma-alumina ($\gamma\text{-Al}_2\text{O}_3$) support with a magnesia (MgO) passivation layer and rhodium oxide (Rh_2O_3). The approximate composition was about 15 wt% Rh_2O_3 , about 5 wt% MgO, and about 80 wt% $\gamma\text{-Al}_2\text{O}_3$. The supported catalyst was prepared by (1) calcining a high surface area $\gamma\text{-Al}_2\text{O}_3$ at 500 °C for 5 hours; (2) impregnating the $\gamma\text{-Al}_2\text{O}_3$ with MgO using the incipient wetness technique with a solution of magnesium nitrate; and obtaining an MgO modified $\gamma\text{-Al}_2\text{O}_3$ support; (3) drying the modified support at 110 °C for 4 hours followed by (4) a second calcination at 900 °C for 2 hours; (5) impregnating the modified support with Rh_2O_3 with the incipient wetness technique from a rhodium nitrate solution; (6) followed by a final drying 110 °C for 4 hours and a (7) a final calcination at 500 °C for 3 hours to obtain a powder of the supported catalyst.

 A microreactor was constructed of a quartz tube with 4mm ID and 6.35 mm OD. About 0.2 g of powder of supported catalyst was placed in the microreactor in a packed bed arrangement.

 Reactants were steam and methane in a steam to carbon ratio of approximately 1 which is stoichiometric within measurement uncertainty. Reactants were flowed through the reactor at temperatures from 650 °C to 900 °C.

 Results are shown in **FIG. 1** for a steam to carbon ratio of 3 with conversion ranging from about 52% to 95% with increasing temperature and selectivity ranging from 22% to 70%.

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